

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property
Organization
International Bureau



(43) International Publication Date
31 December 2003 (31.12.2003)

PCT

(10) International Publication Number
WO 2004/000886 A1

- (51) International Patent Classification⁷: **C08B 37/00**, 37/08, 37/10
- (74) Agent: **SERRAVALLE, Marco**; Serravalle s.a.s., Via B. Cellini, 11, I-20090 Segrate (IT).
- (21) International Application Number: **PCT/EP2003/006446**
- (22) International Filing Date: **18 June 2003 (18.06.2003)**
- (25) Filing Language: **English**
- (26) Publication Language: **English**
- (30) Priority Data:
MI2002A001372 21 June 2002 (21.06.2002) **IT**
- (71) Applicant (*for all designated States except US*): **LABORATORI DERIVATI ORGANICI S.p.A.** [IT/IT]; Via M. Barozzi 4, I-20122 Milano (IT).
- (72) Inventors; and
- (73) Inventors/Applicants (*for US only*): **DE AMBROSI, Luigi** [IT/IT]; Via G. Carducci 8, I-13048 Santhià/Vc (IT). **IANNACONE, Nicola** [IT/IT]; Via Eugenio Chiesa, 2, I-56123 Pisa (IT). **GONELLA, Sergio** [IT/IT]; Via Dolomiti, 1, I-13048 Santhià/Vc (IT). **VISMARA, Elena** [IT/IT]; Via G. Colombo, 81A, I-20133 Milano (IT). **NESTI, Solitario** [IT/IT]; Via Giugnano, 42, I-51030 S. Baronto/PT (IT). **TORRI, Giangiacomo** [IT/IT]; Via G. Colombo, 81A, I-20133 Milano (IT).
- (81) Designated States (*national*): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, OM, PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM, ZW.
- (84) Designated States (*regional*): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IT, LU, MC, NL, PT, RO, SE, SI, SK, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).
- Declaration under Rule 4.17:**
— *of inventorship (Rule 4.17(iv)) for US only*
- Published:**
— *with international search report*
- For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.*

(54) Title: **PROCESS FOR THE PHYSICAL DEPOLYMERIZATION OF GLYCOSAMINOGLYCANS AND PRODUCTS OBTAINED THEREFROM**

(57) Abstract: The invention relates to a process for the depolymerization of glycosaminoglycans characterized by the use of electron beam radiation, optionally in the presence of an organic compound selected from the group consisting of ethers, alcohols, aldehydes, amides and formic acid. The invention also relates to the intermediate depolymerized heparin obtained by the process. The intermediate depolymerized heparin can be dissolved in a buffer solution and fractionated by Gel Permeation for obtaining the desired Molecular Weight.



WO 2004/000886 A1

Process for the physical depolymerization of glycosaminoglycans and products obtained therefrom.

State of the art

5 Glycosaminoglycans are natural products of large pharmaceutical interest. Among the most widely used we can mention heparin, dermatan, heparansulphate and chondroitines.

The molecular weight of the natural products varies considerably and normally ranges from 5 to 40 kDa. It is however known that for certain applications lower molecular
10 weights lead to higher pharmacological activity. The high molecular weight of these compounds often renders impossible their oral administration. Furthermore, it is known that specific activities of glycosaminoglycans are related to relatively short saccharide sequences. Thus, it would be very advantageous to depolymerize glycosaminoglycans reducing the molecular weight without losing the active sites present in the molecule.

15 The chemical depolymerization of glycosaminoglycans is well known in the art and leads to glycosaminoglycans of lower MW but also with a lower S content.

EP 394 971 discloses an enzymatic or chemical depolymerization process. The obtained heparin oligomers have a sulphur content lower than 9%.

WO 90/04607 discloses a depolymerization of heparin and dermatansulfate by the use
20 of H_2O_2 and Cu^{2+} . The ratio $\text{SO}_3^-/\text{COO}^-$ is slightly lower than in the starting heparin.

US 4,987,222 discloses a method for the depolymerization of heparin by the use of gamma rays. The examples disclose the preparation of heparin of Mw around 5,000 Da and with a high S content.

25 **Summary of the invention**

The present invention relates to a physical process for the depolymerization of glycosaminoglycans by the use of electron-beam radiation (EB). It also relates to the glycosaminoglycans obtained by this process.

30 **Detailed description of the invention**

The present invention provides a physical depolymerization process which reduces the molecular weight of glycosaminoglycans without substantially modifying the chemical

structure of the same.

The objective is achieved through use of electron-beam radiation. When using heparin as a starting material, this process results in a low to ultra-low molecular weight heparin characterized by high S content.

- 5 The starting materials to be used in the process according to the present invention are natural glycosaminoglycanes such as heparin, heparansulphate, dermatane and chondroitine. Other suitable starting materials are derivatives of glycosaminoglycanes obtained by known methods. Thus, for example, the N-acetyl or N-sulphate groups of the residues of hexosamine can be transformed into amino groups through N-
- 10 desulphation or N-deacetylation reactions and the sulphate groups of the uronic acids can give rise to epoxy groups through desulphation reactions.

- In another embodiment, it is possible to use as a starting material for the process of the present invention a glycosaminoglycane which has already undergone a depolymerization process either chemical or enzymatic. The use of partly
- 15 depolymerized glycosaminoglycanes is for example relevant in case of heparin which has undergone an acid pretreatment that has as a side effect partial depolymerization, or when depolymerizing functionalized glycosaminoglycanes. The conditions used for the introduction of functional groups are sometimes also causing reduction of the molecular weight of the polysaccharide.

- 20 Thus, not only it is possible to perform both steps by using electron-beam radiation, but it is possible to perform a first depolymerization step by using electron-beam radiation followed by a second step using chemical-enzymatic depolymerization, or to perform a first step of chemical-enzymatic depolymerization followed by electron-beam radiation depolymerization.

- 25 The process of the present invention allows reduction of the molecular weight of the glycosaminoglycane without sensible modification of the chemical structure of the polysaccharide.

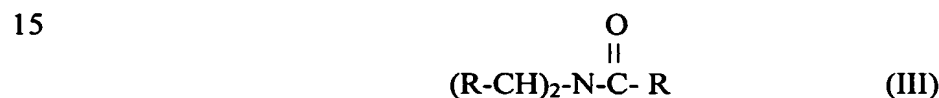
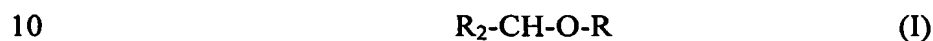
The dose of radiation used in the depolymerization process depends on several factors, e.g. the type of glycosaminoglycanes, the desired final Mw, the energy of the radiation.

- 30 In general, the dose of radiation will vary in the range 400-8,000 kGy, preferably 800-6,000 kGy, more preferably 1,200-5,000 kGy.

Preferably, the electron-beam radiation has an energy comprised between 100 and 1000 keV, most preferably between 100 and 500 keV.

The depolymerization process can be performed in a broad range of temperature, it is however preferred to maintain the temperature between 0 and 50°C, most preferably between 20 and 40 °C.

The depolymerization process according to the invention is preferably performed in aqueous solution, optionally in the presence of an organic compound selected from the group consisting of alcohols, ethers, aldehydes, amides and formic acid. Preferably, the organic compound is selected from compounds of formula I, II and III.



wherein each R is independently selected from the group consisting of H, OH, CHO, C₁-C₆ alkyl and acyl, optionally substituted by oxygen atoms; two R groups optionally join together to form a ring.

Preferred examples of alcohols are: methanol, ethanol, n-propanol, isopropanol, n-butanol, isobutanol, glycerol.

Preferred examples of ethers are: tetrahydrofuran, dioxane, diethylether, tertbutylmethylether, dioxolane.

Examples of aldehydes are formaldehyde, glyoxal, acetaldehyde or stabilized forms thereof (trioxane, glyoxal trimeric dihydrate).

Preferred examples of amides are: N,N-dimethylformamide, N,N-dimethylacetamide, N,N-diethylformamide, N-methylpyrrolidone.

The concentration of glycosaminoglycane in the solution to be submitted to radiation can vary in a broad range. Preferably it is comprised between 2 and 25% w/v, more preferably between 5 and 15%.

After irradiation, the solutions are optionally discolored either by using an oxidizing treatment or by passing them on proper resins. The solution is then generally purified by

precipitation in hydrophilic solvent. The obtained paste can be redissolved in water and lyophilized by vacuum distillation.

It is also possible to fractionate the intermediate depolymerized glycosaminoglycane by Gel Permeation Chromatography. The fractions containing the desired molecular weights are collected, concentrated by ultra filtration and lyophilized.

The process of the present invention is preferably performed by using a dynamic irradiation process.

With the term "dynamic irradiation process" it is meant a process wherein the irradiation is performed on a thin layer of liquid which is fluxing in front of the electron-beam window. In this way, the efficiency of the irradiation process is increased.

The process can be performed either in batch or in continuous mode. The apparatus is preferably formed of a reservoir from which the liquid moves to the irradiation area.

The liquid is then returned to the reservoir.

The exposure of the solution to the electron stream can take place in different ways:

- in front of the window an inclined plane is placed, on which a thin layer of solution flows,
- in front of the window can be placed a system of thin pipes which allow the exposition of the solution to the electrons,
- the solution can flow directly on the window.

The optimal conditions of irradiation are determined through preliminary dosimetry.

The dosimetry has been performed considering the typical conditions of irradiation of the solution in terms of:

- a) properties relating to the beam of electrons, i.e.
 - beam energy (measured in keV)
 - beam current (measured in mA);
- b) properties relating to the geometry of the irradiation, i.e.
 - distance beam source-solution to process,
 - presence of possible shields or other nearby material that can be source of secondary radiation.

The dosimetry is in any case performed for a limited period of time, since the dose administered to the material is directly proportional to the time of the exposition and is determined in static conditions, while in reality the process is dynamic.

- 5 A possible embodiment is represented by Fig.1 wherein the solution is pumped by the pump P from the external tank R to the zone (I). During this transfer, the liquid is cooled down by the heat exchanger F. From (I) the solution falls by gravity following the surface (II), which is preferably porous so as to guaranty the formation of a uniform film on its surface. A pipe connects the area after film (II) with the tank R. The
- 10 irradiation takes place on the film. The flow rate of the pump P determines the characteristics of the film (thickness, residence time in front of the irradiation window).

Experimental section

Characterization of the products

- Molecular weight (Mw) was determined by size exclusion chromatography (European
- 15 Pharmacopoeia 4th ed.: 2.2.30 e 2.2.46 for chromatographic techniques and 01/2002:0828 p. 1297 for method).

β - rays Irradiation

The solution irradiation process takes place inside an electron-beam apparatus.

- 20 The beam is generated by a hot cathode, constituted of a tungsten filament to whom a high voltage is applied.

The beam generation area is posed under vacuum. Such a vacuum is obtained by the combined action of two pumps, a mechanical one and a turbomolecular one.

- The aspiration generated by these two pumps allows the achievement of ideal conditions
- 25 for the free circulation of electrons which. Otherwise, would be slowed down by the air present around the cathode.

The beam reaches the region outside the chamber where it is generated passing through a very thin titanium film (thickness 10 μm). By their passage X rays are also generated.

The solution to be irradiated is placed immediately outside this titanium film, at a distance conveniently as small as possible so that the beam exiting the film is not significantly attenuated and thus the use optimised without useless wastes.

The solution to be irradiated is circulated in proximity of the windows from where the beam exits and it is directly exposed to it. The circulation circuit is provided with an external pumping system. The solution is continuously circulated inside and outside the shielded area and therefore can be regularly sampled and fresh solution for processing can be added.

Example 1

1 l of 10 % sodium heparin solution , free of Heavy metal was prepared. The solution is transferred to the apparatus described in Fig. 1 and the circulation is started in mobile descending phase, over porous glass wool tissue of 1 mm thickness, with a flow rate of 10 l/h by using a peristaltic pump.

When starting the EB irradiation at 5 mA and 300 keV, the cooling system is activated, in order to maintain the temperature between 25 and 35 °C. The depolymerization is monitored by collecting samples, at fixed intervals, on which the Molecular Weight and the composition is determined. The variation in time is shown in Table 1.

The electron beam is stopped and the collected solution undergoes spray-drying to obtain the intermediate product which is fractionated by Gel Permeation.

7.

Table 1

Minutes	> 10.000 Da	kGy	Mw
0	30 %	-	8.364
5	17 %	134	5.941
10	12 %	268	5.050
15	9 %	402	4.523
30	4 %	804	3.682
45	2 %	1.206	3.240
60	1 %	1.608	3.014

Example 2

- 5 The example was conducted under the identical conditions of example 1, but with an intensity of current of 10 mA.

At the end, the electron beam is stopped and the collected solution undergoes spray-drying to obtain the intermediate product which is fractionated by Gel Permeation

10

Table 2

Minutes	> 10.000	kGy	Mw
0	30 %	-	8.364
5	12 %	268	4.888
10	7 %	536	4.053
15	4 %	804	3.526
30	2 %	1.608	3.040
45	1 %	2.412	2.852
60	-	3.216	2.716

Example 3

The example was conducted under the identical conditions of example 1, but with a beam energy of 150 keV and a current of 5 mA. The results are reported in Table 3.

Table 3

Minutes	> 10.000	kGy	Mw
0	30 %	-	8.364
5	24 %	161	7163
10	21 %	322	6542
15	20 %	483	6337
30	17 %	966	5968
45	16 %	1449	6333
60	13 %	1932	5681
75	10 %	2415	5235
90	8 %	2898	4806

Example 4

- 5 The example was conducted under the identical condition of example 1, but with the addition of 0.4 %v/v of isopropanol. Table 4 reports the obtained results.

Table 4

Minutes	> 10.000 Da	kGy	Mw
0	30 %	-	8.364
5	20 %	134	6265
10	16 %	268	5653
15	12 %	402	4851
30	5 %	804	3760
45	3 %	1.206	3298
60	1 %	1.608	3018
75	1 %	2010	2855
80	-	2144	2780

Example 5

The example was conducted under the identical condition of example 2, but with the addition of 0.4 %v/v of isopropanol. Table 5 reports the obtained results.

5

Table 5

Minutes	> 10.000 Da	kGy	Mw
0	30 %	-	8.364
5	16 %	268	5625
10	10 %	536	4626
15	7 %	804	4043
20	4 %	1072	3559
25	3 %	1.340	3289
30	3 %	1.608	3261
45	1 %	2412	2913
55	1 %	2948	2921

Claims

1. Process for the depolymerization of glycosaminoglycanes characterized by the use of electron-beam radiation.
2. Process according to claim 1 performed by using a dynamic irradiation process.
3. Process according to claims 1-2 wherein the glycosaminoglycane is heparin.
4. Process according to claims 1-3 wherein the electron-beam radiation has an energy comprised between 100 and 1000 keV.
5. Process according to claims 1-4 wherein the process is performed in aqueous solution.
6. Process for the depolymerization of glycosaminoglycanes according to claim 5 in the presence of an organic compound represented by formulas I, II and III:



wherein each R is independently selected from the group consisting of H, OH, CHO, C₁-C₆ alkyl and acyl, optionally substituted by oxygen atoms; two R groups optionally join together to form a ring.

7. Process according to claim 6 wherein the organic compound is selected from the group consisting of methanol, ethanol, n-propanol, isopropanol, n-butanol, isobutanol, glycerol, tetrahydrofurane, dioxane, diethylether, tertbutylmethylether, dioxolane, formaldehyde, glyoxal, acetaldehyde, N,N-dimethylformamide, N,N-dimethylacetamide, N,N-diethylformamide, N-methylpyrrolidone.
8. Process according to claims 6-7 wherein the amount of organic compound varies between 0.1 and 5%.
9. Process according to claims 1-7 wherein the amount of radiation used is comprised between 400 and 8,000 kGy.

10. Glycosaminoglycanes obtainable by the process of claims 1-9.

INTERNATIONAL SEARCH REPORT

International Application No

PCT/EP/06446

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 C08B37/00 C08B37/08 C08B37/10

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 C08B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, PAJ, CHEM ABS Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	<p>DATABASE CHEMABS 'Online! CHEMICAL ABSTRACTS SERVICE, COLUMBUS, OHIO, US; "Process for preparing low molecular polysaccharide and oligosaccharide thereof by photochemical or ultrasonic degradation of polysaccharides" retrieved from STN Database accession no. 136:134987 XP002255493 abstract & KR 2000 012 173 A (S. KOREA) 6 March 2000 (2000-03-06)</p> <p style="text-align: center;">---</p> <p style="text-align: center;">-/--</p>	1-10

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

* Special categories of cited documents:

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the international filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

- *T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- *X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- *Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- *G* document member of the same patent family

Date of the actual completion of the international search

24 September 2003

Date of mailing of the international search report

10/10/2003

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax: (+31-70) 340-3016

Authorized officer

Mazet, J-F

INTERNATIONAL SEARCH REPORT

International Application No

PCT/EP/06446

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	DATABASE CHEMABS 'Online! CHEMICAL ABSTRACTS SERVICE, COLUMBUS, OHIO, US; "Method for manufacturing low molecular polysaccharide and oligosaccharide thereof" retrieved from STN Database accession no. 136:185632 XP002255494 abstract & KR 2000 036 332 A (S. KOREA) 5 July 2000 (2000-07-05) ---	1-10
A	EP 0 269 937 A (MEDIOLANUM FARMACEUTICI SRL) 8 June 1988 (1988-06-08) claims A & US 4 987 222 A (DE AMBROSI ET AL.) 22 January 1991 (1991-01-22) cited in the application ---	1-10
A	DATABASE WPI Section Ch, Week 199514 Derwent Publications Ltd., London, GB; Class B04, AN 1995-101801 XP002255467 & JP 07 025772 A (JAPAN ATOMIC ENERGY RES INST), 27 January 1995 (1995-01-27) abstract ---	1-10
A	GB 1 255 723 A (DOW CHEMICAL COMPANY) 1 December 1971 (1971-12-01) page 1, line 37 - line 59; claims ---	1-10
A	WO 95 04778 A (PLANET POLYMER TECH INC ;PETCAVICH ROBERT J (US)) 16 February 1995 (1995-02-16) claims ---	1
A	US 2002/010152 A1 (DE AMBROSI ET AL.) 24 January 2002 (2002-01-24) claims -----	1

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/EP/06446

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
KR 2000012173	A	06-03-2000	NONE	
KR 2000036332	A	05-07-2000	NONE	
EP 269937	A	08-06-1988	IT 1213384 B AT 60924 T AU 603622 B2 AU 8160987 A CA 1305134 C DE 3768074 D1 DK 602387 A EP 0269937 A2 FI 875185 A ,B, GR 3001670 T3 JP 1877327 C JP 5088881 B JP 63213502 A NO 874777 A PT 86191 A ,B US 4987222 A	20-12-1989 15-03-1991 22-11-1990 26-05-1988 14-07-1992 28-03-1991 15-09-1988 08-06-1988 25-05-1988 23-11-1992 07-10-1994 24-12-1993 06-09-1988 25-05-1988 01-12-1987 22-01-1991
JP 7025772	A	27-01-1995	NONE	
GB 1255723	A	01-12-1971	DE 1928045 A1	02-01-1970
WO 9504778	A	16-02-1995	AU 679780 B2 AU 7560394 A CN 1129005 A EP 0714419 A1 FI 960610 A JP 7165951 A WO 9504778 A1 US 5505830 A	10-07-1997 28-02-1995 14-08-1996 05-06-1996 09-02-1996 27-06-1995 16-02-1995 09-04-1996
US 2002010152	A1	24-01-2002	IT MI972835 A1	21-06-1999